

Hydrochar and Humic Acid as Template of ZnAl Layered Double Hydroxide for Adsorption of Phenol

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Abstract

The adsorbents potential ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid were prepared using the coprecipitation method. The adsorbents were characterization by XRD, FTIR, and BET analysis. XRD peaks of ZnAl-LDH at 10.29°, 20.07°, 29.59°, 32.12°, 34.02°, 48.06°, and 60.16°. The FTIR absorption peak was observed at 3400-3500 cm⁻¹, 1600-1700 cm⁻¹, 1381 cm⁻¹, 1000 cm⁻¹, 500-700 cm⁻¹. All adsorbents exhibited N₂ adsorption-desorption isotherms type IV classified as a mesoporous structure (pore size= 2-50 nm). The surface areas of composites were higher than LDH and following order: ZnAl-Hydrochar > ZnAl-Humic acid > ZnAl-LDH. The kinetic parameter showed the pseudo-second-order kinetics model. The maximum adsorption capacity of ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid were 48.077 mg/g, 90.090 mg/g, 94.340 mg/g, respectively; with Freundlich isotherm model. Reusability after 5 times of ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid in the range 49.81-0.890%, 95.92-9.84%, and 70.02-5.72%, respectively. The adsorbent can be used up to 3 times.

Keywords

Hydrochar, Humic Acid, LDH, Adsorption, Phenol, Regeneration

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1. INTRODUCTION

Water is a basic human need to carry out activities. Drinking water used must meet physical, chemical, and biological requirements. Recently, rivers as water sources have been polluted by various kinds of waste, ranging from household and industrial to domestic waste (Selvanathan et al., 2017). The waste is not handled correctly, so the water becomes polluted (Chaari et al., 2020). One of the most dangerous wastes for the aquatic environment is phenol waste. Several industries that have the potential to produce phenol waste include the petroleum refining, textile, gas, pharmaceutical, and petrochemical industries, coal processing, pharmaceuticals, polymer resins, pesticides, and household industries that produce liquid phenol waste (Desmiarti et al., 2019; Zhang et al., 2021).

Phenol is a dangerous organic compound with a high level of toxicity, which can cause harm to humans and biota (De la Luz-Asunción et al., 2015; Dehbi et al., 2020; Dehmani et al., 2021; Girish and Ramachandra Murty, 2014) and accumulates in the environment. The limit of phenol concentration

is 1.0 mg/L in water (Xie et al., 2020). Thus, developing an effective treatment to removal of phenol is necessary before being discharged to environment. Various methods have been proposed for phenol wastewater treatment, including oxidation, membrane separation, biodegradation, ion exchange, and adsorption (Tshemese et al., 2021). Adsorption is one technique for removal of phenol because it is fast, cost-effective, easy handling, regeneration, high selectivity, and high efficiency (Badhai et al., 2020; Ho and Adnan, 2021).

One of the materials used for water treatment in the adsorption process is layered double hydroxide (LDH). This material has become a material that has been widely developed because of its uniqueness and good absorption. Its application in water treatment as an adsorbent has excellent potential due to its low cost, exchangeable anionic features, and large surface area (Bouteraa et al., 2020; Zubair et al., 2021). According to Vithanage et al. (2020), LDH is adsorbent in water treatment applications to remove organic, inorganic species, dyestuffs, and toxic metal contaminants. Rathee et al. (2019) reported that LDH, which was applied as an adsorbent, had limitations in

the regeneration process. Therefore, the double-layer hydroxyl needs to be modified with a carbon-based support material to form a composite.

Layered double hydroxide NiAl, ZnAl, and MgAl composited with carbon-based materials such as chitosan were effectively to remove congo red, and the ability of the composite to be used repeatedly was stable until the seventh cycle in the regeneration process (Siregar et al., 2021). Based on the literature, it can be concluded that carbon-based supporting materials to form composites, such as hydrochar and humic acid, are suitable for use in layered double hydroxide. According to Zubair et al. (2021), layered double hydroxide modified with carbon-based support material showed significant results, namely an increase in physicochemical characteristics such as surface area, structural stability, functional groups, and the resulting adsorption characteristics.

In this study, the synthesis of ZnAl-LDH using the coprecipitation method and the preparation of ZnAl composites with hydrochar and humic acid were carried out. The synthesized and prepared materials were characterized using X-Ray Diffraction (XRD), Fourier Transform Infra-Red (FTIR), and Brunauer Emmet Teller (BET). Furthermore, the material will be applied as an adsorbent to adsorb phenol by studying various parameters including pH, contact time, temperatures, initial concentration, and regeneration.

2. EXPERIMENTAL SECTION

2.1 Chemicals and Instrumentation

The chemicals were used, including zinc nitrate hexahydrate ($\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$), aluminum nitrate nonahydrate ($\text{Al}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$), sodium carbonate (Na_2CO_3), humic acid, hydrochar, hydrogen chloride (HCl), distilled water (H_2O), sodium hydroxide (NaOH), phenol ($\text{C}_6\text{H}_5\text{OH}$), 4-aminoantipyrine ($\text{C}_{11}\text{H}_{13}\text{N}_3\text{O}$), potassium hexacyanoferrate(III) ($\text{K}_3[\text{Fe}(\text{CN})_6]$), and acetate buffer solution (CH_3COONa) pH 10. Instrumentation was used in this study, including X-Ray Diffraction (XRD), Brunauer Emmet Teller (BET), and Fourier Transform Infra-Red (FTIR).

2.2 Synthesis of ZnAl-LDH

ZnAl-LDH synthesis was carried out with 100 mL $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ 0.75 M mixed with 100 mL $\text{Al}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ 0.25 M, then dripped into 50 mL NaOH 2 M solution (Mohadi et al., 2022). The mixture was adjusted to pH 10, then stirred for 20 h at 353 K. After stirring, the precipitate was filtered and rinsed using distilled water to remove impurities. The precipitate was dried using an oven.

2.3 Preparation of ZnAl-Hydrochar and ZnAl-Humic Acid

ZnAl composites were prepared using the coprecipitation method with constant pH. A total of 15 mL of 0.75 M Zn solution and 15 mL of 0.25 M Al solution were mixed, and the pH was adjusted to pH 10. The mixture was stirred for 1 h until homogeneous, and a gel was formed, then 3 g of humic acid/hydrochar was added. The solution was kept at 353 K for

3 days. The precipitate from the preparation was filtered and dried using an oven.

2.4 Adsorption of Phenol

Phenol is a colorless solution, so it must be complexed before being measured using a UV-Vis spectrophotometer (Xie et al., 2020). 1 mL of phenol solution was put in a beaker, then 0.1 mL of 4-aminoantipyrine 2% was added, 0.1 mL of potassium hexacyanoferrate (III) 8%, 1 mL of pH 10 buffer solution, and 3 mL of distilled water were added. Then homogenized and allowed to stand for 5 min. The maximum wavelength of phenol after complexing is 510 nm.

2.5 Effect of pH

Adsorbent (0.05 g) was put into a 100 mL beaker filled with 50 mL of phenol solution, each at a concentration of 20 mg/L with a variation of pH 2-11 with stirring for 2 h.

2.6 Effect of Contact Time

Adsorbent (0.05 g) was added to 50 mL of 20 mg/L phenol solution, then stirred with variations contact time (0-180 min). The adsorbent was separated from the phenol solution.

2.7 Effect of Initial Concentration and Temperatures

Adsorbent (0.05 g) was added 50 mL of phenol solution with various initial concentrations (10 mg/L, 20 mg/L, 30 mg/L, 40 mg/L and 50 mg/L and various temperatures (303 K, 313 K, 323 K, and 333 K). The solution was stirred for 2 h.

2.8 Reusability of Adsorbents

The adsorption process for phenol is carried out before being used repeatedly as an adsorbent. After that, the desorption of phenol solution using an ultrasonic device. The regeneration process is carried out by adding 50 mg/L of 50 mL phenol solution to adsorbent that has gone through the desorption process.

3. RESULT AND DISCUSSION

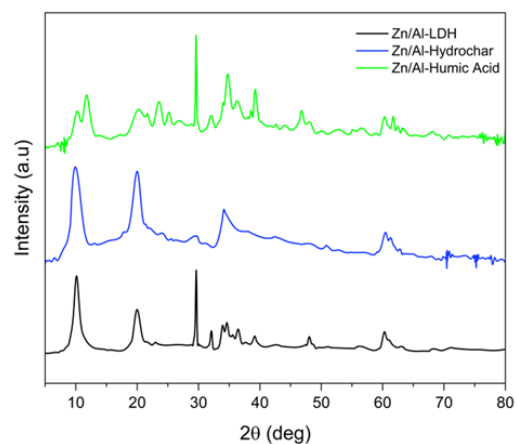


Figure 1. XRD Diffractogram of Adsorbents

XRD patterns of ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid is displayed in Figure 1. ZnAl-LDH peaks at 10.29° , 20.07° , 29.59° , 32.12° , 34.02° , 48.06° , and 60.16° were indexed to (003), (006), (101), (012), (015), (107), and (110) corresponding to JCPDS No 05-0669 (Elhalil et al., 2017). The peaks at 10.29° and 60.16° indicated the anion in the interlayer of layered double hydroxide. After ZnAl-LDH was composited with hydrochar and humic acid, the peak at 20.3° indicated the humic acid, while the diffraction peaks of hydrochar at peaks 18.0° . The characteristic peaks of the constituents ZnAl-LDH, hydrochar, and humic acid indicated that the preparation of the composite has been successful.

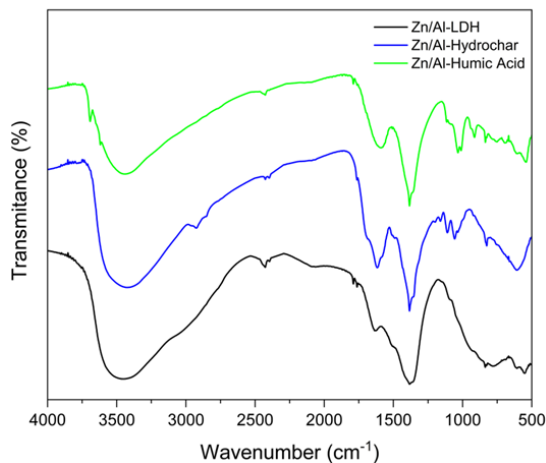


Figure 2. FTIR Spectra of Adsorbents

Figure 2 shows the FTIR spectra of ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid. The absorption peak was observed at $3400\text{-}3500\text{ cm}^{-1}$ assigned to O-H vibration from water in LDH (Li et al., 2020). The peak at $1600\text{-}1700\text{ cm}^{-1}$ indicated vibration of -OH and carbonyl (COO) (Rashid et al., 2017). The peak at 1381 cm^{-1} corresponds to N-O from nitrate (Palapa et al., 2021). The new peak around 1000 cm^{-1} at ZnAl-Hydrochar and ZnAl-Humic acid indicated C-O stretching from hydrochar and humic acid (Lu et al., 2019; Shao et al., 2022). The peak at $500\text{-}700\text{ cm}^{-1}$ assigns to metal-oxide in LDH (Ahmad et al., 2022b).

Textural properties of ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid give in Figure 3. All adsorbents exhibited N_2 adsorption-desorption isotherms type IV classified as a mesoporous structure (pore size = 2-50 nm) (Cao et al., 2022). In line with the data in Table 1, the pore size of adsorbent is 4-27 nm. The surface areas of composites were higher than LDH and were in the following order: ZnAl-Hydrochar > ZnAl-Humic acid > ZnAl-LDH. The pore volume of ZnAl-Hydrochar was higher than ZnAl-Humic acid and ZnAl-LDH. Thus, the surface area is directly proportional to the pore volume.

The effect of pH in adsorption phenol was displayed in Figure 4. pH is one of the key parameters in adsorption. pH

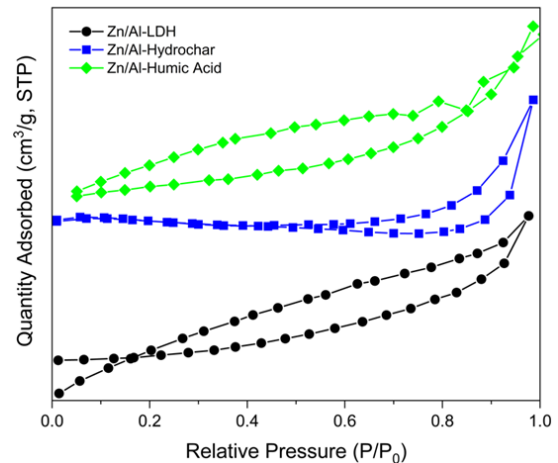


Figure 3. N_2 Adsorption-desorption Isotherms

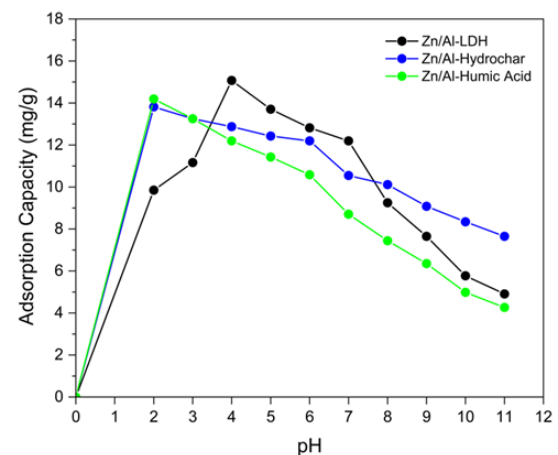


Figure 4. Effect of pH

optimum of ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid was at pH 4, 2, and 2, respectively. Under acidic conditions, phenol adsorption is better because the phenol molecules do not dissociate, thereby reducing electrostatic repulsion and hydrogen bonding being the primary interaction (Asnaoui et al., 2022).

Kinetic parameters adsorption of phenol is shown in Figure 5. The pseudo-first-order (PFO) and pseudo-second-order (PSO) kinetic models were determined through the highest linear regression value. Based on Table 2, ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid followed the PSO kinetics model (R^2 closer to 1). PSO model assumes that the active site of the adsorbent is available more than the possible bond between the adsorbent and the adsorbate that occurs (de Farias et al., 2022).

Determination isotherm model seen the linear regression value (R^2) which is closer to 1. ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid tend to follow the Freundlich isotherm model because the R^2 value is closer to 1 compared to the

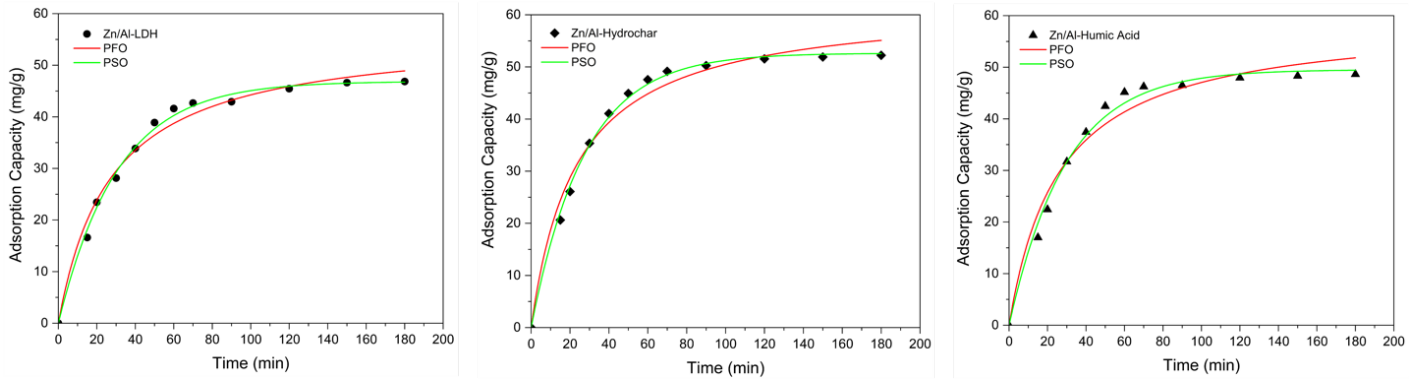


Figure 5. Effect of Contact Time

Table 1. BET Analysis of Adsorbents

| Adsorbents | Surface Area (m ² /g) | Pore Size (nm), BJH | Pore Volume (cm ³ /g), BJH |
|-----------------|----------------------------------|---------------------|---------------------------------------|
| ZnAl-LDH | 1.968 | 27.687 | 0.006 |
| ZnAl-Hydrochar | 29.874 | 24.420 | 0.042 |
| ZnAl-Humic Acid | 16.425 | 4.811 | 0.039 |

Table 2. Kinetics Parameters the Adsorption Process

| Kinetic Parameter | Parameters | Adsorbents | | |
|-------------------|----------------------------|------------|----------------|-----------------|
| | | ZnAl-LDH | ZnAl-Hydrochar | ZnAl-Humic Acid |
| PFO | $Q_{e_{exp}}$ (mg/g) | 46.845 | 52.228 | 48.627 |
| | $Q_{e_{calc}}$ (mg/g) | 48.228 | 44.627 | 41.295 |
| | k_1 (min ⁻¹) | 0.033 | 0.034 | 0.034 |
| | R^2 | 0.965 | 0.989 | 0.969 |
| PSO | $Q_{e_{exp}}$ (mg/g) | 46.845 | 52.228 | 48.627 |
| | $Q_{e_{calc}}$ (mg/g) | 56.644 | 59.524 | 56.497 |
| | k_2 (min ⁻¹) | 0.001 | 0.001 | 0.001 |
| | R^2 | 0.993 | 0.993 | 0.986 |

Table 3. Isotherm Parameters the Adsorption Process

| Adsorbents | T (K) | Langmuir | | | Freundlich | | |
|-----------------|-------|------------------|----------------|----------------|------------|----------------|----------------|
| | | Q _{max} | k _L | R ² | n | k _F | R ² |
| ZnAl-LDH | 303 | 20.492 | 0.167 | 0.974 | 5.149 | 15.765 | 0.994 |
| | 313 | 48.077 | 0.063 | 0.844 | 1.866 | 5.338 | 0.847 |
| | 323 | 43.487 | 0.140 | 0.930 | 2.482 | 9.643 | 0.822 |
| | 333 | 42.553 | 0.332 | 0.984 | 3.221 | 15.191 | 0.855 |
| ZnAl-Hydrochar | 303 | 27.027 | 0.019 | 0.961 | 1.989 | 6.703 | 0.947 |
| | 313 | 85.470 | 0.012 | 0.956 | 1.164 | 2.078 | 0.957 |
| | 323 | 75.188 | 0.038 | 0.7984 | 1.473 | 4.248 | 0.954 |
| | 333 | 90.090 | 0.071 | 0.8516 | 1.900 | 7.579 | 0.943 |
| ZnAl-Humic Acid | 303 | 26.882 | 0.078 | 0.969 | 3.837 | 12.552 | 0.989 |
| | 313 | 44.444 | 0.053 | 0.944 | 1.678 | 4.281 | 0.975 |
| | 323 | 64.935 | 0.049 | 0.900 | 1.616 | 5.018 | 0.962 |
| | 333 | 94.340 | 0.077 | 0.911 | 1.987 | 8.468 | 0.968 |

Table 4. Several Adsorbents to Adsorption of Phenol

| Adsorbent | Q _{max} (mg/g) | References |
|--|-------------------------|--------------------------------------|
| Lignite | 6.216 | (Liu et al., 2021) |
| Tea waste biomass | 7.62 | (Gupta and Balomajumder, 2015) |
| MAG-CTAB-KH550 | 56.13 | (Ge et al., 2018) |
| Bentonite | 23.64 | (Ahmadi and Igwegbe, 2018) |
| Fe-Biochar | 39.23 | (Dong et al., 2021) |
| ZnCl ₂ -BFAC | 17.02 | (Sathya Priya and Sureshkumar, 2020) |
| Clarified sludge from basic oxygen furnace | 1.052 | (Mandal and Das, 2019) |
| α -Fe ₂ O ₃ | 21.93 | (Dehmani and Abouarnadasse, 2020) |
| Activated carbon | 75.81 | (da Silva et al., 2022) |
| ZnAl-LDH | 48.077 | This study |
| ZnAl-Hydrochar | 90.090 | This study |
| ZnAl-Humic Acid | 94.340 | This study |

Table 5. Adsorption Thermodynamic Parameter

| Adsorbents | ΔH (kJ/mol) | ΔS (J/K.mol) | ΔG (kJ/mol) | | | | R ² |
|-----------------|---------------------|----------------------|---------------------|--------|--------|--------|----------------|
| | | | 303 K | 313 K | 323 K | 333 K | |
| ZnAl-LDH | 51.180 | 0.171 | -0.586 | -2.294 | -4.003 | -5.711 | 0.985 |
| ZnAl-Hydrochar | 33.152 | 0.110 | -0.224 | -1.326 | -2.427 | -3.529 | 0.993 |
| ZnAl-Humic Acid | 33.821 | 0.133 | -0.488 | -1.620 | -2.752 | -3.885 | 0.988 |

Langmuir isotherm model (See Table 3). Freundlich isotherm assumes that the adsorption process is physisorption and occurs in multilayers (Jain et al., 2022). The maximum adsorption capacity of ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid were 48.077 mg/g, 90.090 mg/g, 94.340 mg/g, respectively. The comparison of adsorption capacity with other adsorbents can be seen in Table 4.

The thermodynamic parameters determined in the adsorption include enthalpy (ΔH), entropy (ΔS), and Gibbs free energy (ΔG) as presented in Table 5. The enthalpy (ΔH) is positive in the range of 31-51 kJ/mol, this indicates that the reaction that occurs is endothermic (Dehmani et al., 2020). The entropy (ΔS) is positive in the range of 0.110 - 0.171 J/mol.K, this indicates that the degree of disorder is small during the adsorption process (Zhang et al., 2022). The Gibbs free energy (ΔG) is negative, indicating that adsorption of phenol is spontaneous (Ahmad et al., 2022a).

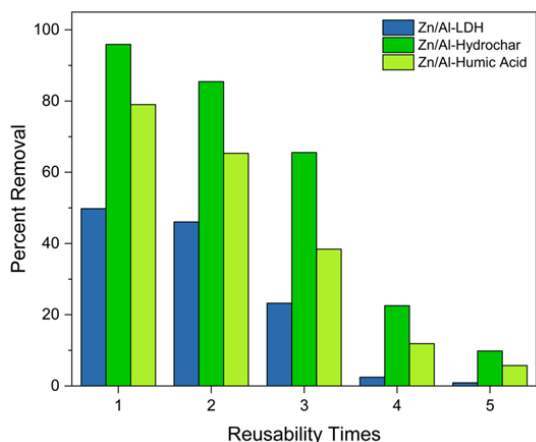


Figure 6. Reusability of Adsorbents

Reusability of adsorbent is the repeated use of the adsorbent by removing the adsorbate from the adsorbent (Qu et al., 2022). Based on Figure 6, reusability after 5 times of ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid in the range 49.81-0.890%, 95.92-9.84%, and 70.02-5.72%, respectively. The percentage of reusability decreases with the frequent adsorption process. The adsorbent can be used up to 3 times.

4. CONCLUSION

In summary, ZnAl-LDH, ZnAl-Hydrochar, and ZnAl-Humic acid were successfully prepared. The adsorbents were characterized by XRD, FTIR, and BET analysis. The maximum adsorption capacity is 94.340 mg/g on ZnAl-Humic acid. Parameters such as pH, contact time, concentration, temperature, and regeneration affected to adsorption process. Kinetic and isotherm data were fitted to the PSO kinetic model and Freundlich isotherm model, respectively. The adsorbent can be used up to 3 times in the adsorption of phenol.

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REFERENCES

- Ahmad, N., F. S. Arsyad, I. Royani, and A. Lesbani (2022a). Selectivity of Malachite Green on Cationic Dye Mixtures Toward Adsorption on Magnetite Humic Acid. *Environment and Natural Resources Journal*, **20**(6); 1-10
- Ahmad, N., A. Wijaya, E. S. F. Amri, F. S. Arsyad, R. Mohadi, and A. Lesbani (2022b). Catalytic Oxidative Desulfurization of Dibenzothiophene by Composites Based Ni/Al-Oxide. *Science and Technology Indonesia*, **7**(3); 385-391
- Ahmadi, S. and C. A. Igwegbe (2018). Adsorptive Removal of Phenol and Aniline by Modified Bentonite: Adsorption Isotherm and Kinetics Study. *Applied Water Science*, **8**(6); 1-8
- Asnaoui, H., Y. Dehmani, M. Khalis, and E.-K. Hachem (2022). Adsorption of Phenol from Aqueous Solutions by Na-bentonite: Kinetic, Equilibrium and Thermodynamic Studies. *International Journal of Environmental Analytical Chemistry*, **102**(13); 3043-3057
- Badhai, P., S. Kashyap, and S. K. Behera (2020). Adsorption of Phenol Red onto GO-Fe₃O₄ Hybrids in Aqueous Media. *Environmental Nanotechnology, Monitoring and Management*, **13**; 100282
- Bouteraa, S., F. B. D. Saiah, S. Hamouda, and N. Bettahar (2020). Zn-M-CO₃ Layered Double Hydroxides (M= Fe, Cr, or Al): Synthesis, Characterization, and Removal of Aqueous Indigo Carmine. *Bulletin of Chemical Reaction Engineering and Catalysis*, **15**(1); 43-54
- Cao, Y., Y. Wang, F. Zhou, J. Huang, and M. Xu (2022). Acylamino-functionalized Hyper-cross-linked Polymers for Efficient Adsorption Removal of Phenol in Aqueous Solution. *Separation and Purification Technology*, **303**; 122229
- Chaari, I., A. Touil, and M. Medhioub (2020). Adsorption-desorption of Phenolic Compounds from Olive Mills Wastewater Using Tunisian Natural Clay. *Chinese Journal of Chemical Engineering*, **40**; 287-292
- da Silva, M. C., C. Schnorr, S. F. Lütke, S. Knani, V. X. Nascimento, É. C. Lima, P. S. Thue, J. Vieillard, L. F. Silva, and G. L. Dotto (2022). KOH Activated Carbons from Brazil Nut Shell: Preparation, Characterization, and Their Application in Phenol Adsorption. *Chemical Engineering Research and Design*, **187**; 387-396
- de Farias, M. B., P. Prediger, and M. G. A. Vieira (2022). Conventional and Green-synthesized Nanomaterials Applied for the Adsorption and/or Degradation of Phenol: A Recent Overview. *Journal of Cleaner Production*, **367**; 132980
- De la Luz-Asunción, M., V. Sánchez-Mendieta, A. Martínez-Hernández, V. Castaño, and C. Velasco-Santos (2015). Adsorption of Phenol from Aqueous Solutions by Carbon

- Nanomaterials of One and Two Dimensions: Kinetic and Equilibrium Studies. *Journal of Nanomaterials*, **2015**
- Dehbi, A., Y. Dehmani, H. Omari, A. Lammini, K. Elazhari, S. Abouarnadasse, and A. Abdallaoui (2020). Comparative Study of Malachite Green and Phenol Adsorption on Synthetic Hematite Iron Oxide Nanoparticles (α -Fe₂O₃). *Surfaces and Interfaces*, **21**; 100637
- Dehmani, Y. and S. Abouarnadasse (2020). Study of the Adsorbent Properties of Nickel Oxide for Phenol Depollution. *Arabian Journal of Chemistry*, **13**(5); 5312–5325
- Dehmani, Y., A. A. Alrashdi, H. Lgaz, T. Lamhasni, S. Abouarnadasse, and I.-M. Chung (2020). Removal of Phenol from Aqueous Solution by Adsorption onto Hematite (α -Fe₂O₃): Mechanism Exploration from Both Experimental and Theoretical Studies. *Arabian Journal of Chemistry*, **13**(5); 5474–5486
- Dehmani, Y., O. El Khalki, H. Mezougane, and S. Abouarnadasse (2021). Comparative Study on Adsorption of Cationic Dyes and Phenol by Natural Clays. *Chemical Data Collections*, **33**; 100674
- Desmiarti, R., M. Martynis, Y. Trianda, F. Li, A. Viqri, and T. Yamada (2019). Phenol Adsorption in Water by Granular Activated Carbon from Coconut Shell. *Chemical Engineering*, **10**(8); 1488–1497
- Dong, F. X., L. Yan, X. H. Zhou, S. T. Huang, J. Y. Liang, W. X. Zhang, Z. W. Guo, P. R. Guo, W. Qian, and L. J. Kong (2021). Simultaneous Adsorption of Cr (VI) and Phenol by Biochar-based Iron Oxide Composites in Water: Performance, Kinetics and Mechanism. *Journal of Hazardous Materials*, **416**; 125930
- Elhalil, A., R. Elmoubarki, A. Machrouhi, M. Sadiq, M. Abdennouri, S. Qourzal, and N. Barka (2017). Photocatalytic Degradation of Caffeine by ZnO-ZnAl₂O₄ Nanoparticles Derived from LDH Structure. *Journal of Environmental Chemical Engineering*, **5**(4); 3719–3726
- Ge, M., X. Wang, M. Du, G. Liang, G. Hu, and J. A. SM (2018). Adsorption Analyses of Phenol from Aqueous Solutions Using Magadiite Modified with Organo-functional Groups: Kinetic and Equilibrium Studies. *Materials*, **12**(1); 96
- Girish, C. and V. Ramachandra Murty (2014). Adsorption of Phenol from Aqueous Solution Using Lantana camara, Forest Waste: Kinetics, Isotherm, and Thermodynamic Studies. *International Scholarly Research Notices*, **2014**; 1–16
- Gupta, A. and C. Balomajumder (2015). Simultaneous Removal of Cr (VI) and Phenol from Binary Solution Using Bacillus sp. Immobilized onto Tea Waste Biomass. *Journal of Water Process Engineering*, **6**; 1–10
- Ho, Z. H. and L. A. Adnan (2021). Phenol Removal from Aqueous Solution by Adsorption Technique Using Coconut Shell Activated Carbon. *Tropical Aquatic and Soil Pollution*, **1**(2); 98–107
- Jain, M., S. A. Khan, A. Sahoo, P. Dubey, K. K. Pant, Z. M. Ziora, and M. A. Blaskovich (2022). Statistical Evaluation of Cow-dung Derived Activated Biochar for Phenol Adsorption: Adsorption Isotherms, Kinetics, and Thermodynamic Studies. *Bioresource Technology*, **352**; 127030
- Li, A., H. Deng, C. Ye, and Y. Jiang (2020). Fabrication and Characterization of Novel ZnAl-layered Double Hydroxide for the Superadsorption of Organic Contaminants from Wastewater. *ACS Omega*, **5**(25); 15152–15161
- Liu, X., Y. Tu, S. Liu, K. Liu, L. Zhang, G. Li, and Z. Xu (2021). Adsorption of Ammonia Nitrogen and Phenol onto the Lignite Surface: An Experimental and Molecular Dynamics Simulation Study. *Journal of Hazardous Materials*, **416**; 125966
- Lu, S., W. Liu, Y. Wang, Y. Zhang, P. Li, D. Jiang, C. Fang, and Y. Li (2019). An Adsorbent Based on Humic Acid and Carboxymethyl Cellulose for Efficient Dye Removal from Aqueous Solution. *International Journal of Biological Macromolecules*, **135**; 790–797
- Mandal, A. and S. K. Das (2019). Phenol Adsorption from Wastewater Using Clarified Sludge from Basic Oxygen Furnace. *Journal of Environmental Chemical Engineering*, **7**(4); 103259
- Mohadi, R., P. M. S. B. N. Siregar, N. R. Palapa, and A. Lesbani (2022). Preparation of Zn/Al-chitosan Composite for the Selective Adsorption of Methylene Blue Dye in Water. *Makara Journal of Science*, **26**(2); 128–136
- Palapa, N. R., T. Taher, A. Wijaya, and A. Lesbani (2021). Modification of Cu/Cr Layered Double Hydroxide by Keggin Type Polyoxometalate as Adsorbent of Malachite Green from Aqueous Solution. *Science and Technology Indonesia*, **6**(3); 209–217
- Qu, Y., L. Qin, X. Liu, and Y. Yang (2022). Magnetic Fe₃O₄/ZIF-8 Composite as an Effective and Recyclable Adsorbent for Phenol Adsorption from Wastewater. *Separation and Purification Technology*, **294**; 121169
- Rashid, M., N. T. Price, M. A. G. Pinilla, and K. E. O'Shea (2017). Effective Removal of Phosphate from Aqueous Solution Using Humic Acid Coated Magnetite Nanoparticles. *Water Research*, **123**; 353–360
- Rathee, G., A. Awasthi, D. Sood, R. Tomar, V. Tomar, and R. Chandra (2019). A new Biocompatible Ternary Layered Double Hydroxide Adsorbent for Ultrafast Removal of Anionic Organic Dyes. *Scientific Reports*, **9**(1); 1–14
- Sathya Priya, D. and M. Sureshkumar (2020). Synthesis of Borassus Flabellifer Fruit Husk Activated Carbon Filter for Phenol Removal from Wastewater. *International Journal of Environmental Science and Technology*, **17**(2); 829–842
- Selvanathan, M., K. T. Yann, C. H. Chung, A. Selvarajoo, S. K. Arumugasamy, and V. Sethu (2017). Adsorption of Copper (II) Ion from Aqueous Solution Using Biochar Derived from Rambutan (nepheliumlappaceum) Peel: Feedforward Neural Network Modelling Study. *Water, Air, and Soil Pollution*, **228**(8); 1–19
- Shao, Y., M. Bao, W. Huo, R. Ye, Y. Liu, and W. Lu (2022). Production of Artificial Humic Acid from Biomass Residues by a Non-catalytic Hydrothermal Process. *Journal of Cleaner Production*, **335**; 130302

- Siregar, P. M. S. B. N., N. Juleanti, A. Wijaya, N. R. Palapa, R. Mohadi, and A. Lesbani (2021). Mg/Al-CH, Ni/Al-CH and Zn/Al-CH, as Adsorbents for Congo Red Removal in Aqueous Solution. *Communications in Science and Technology*, **6**(2); 74–79
- Tshemese, S. J., W. Mhike, and S. M. Tichapondwa (2021). Adsorption of Phenol and Chromium (VI) from Aqueous Solution Using Exfoliated Graphite: Equilibrium, Kinetics and Thermodynamic Studies. *Arabian Journal of Chemistry*, **14**(6); 103160
- Vithanage, M., A. Ashiq, S. Ramanayaka, and A. Bhatnagar (2020). Implications of Layered Double Hydroxides Assembled Biochar Composite in Adsorptive Removal of Contaminants: Current Status and Future Perspectives. *Science of The Total Environment*, **737**; 139718
- Xie, B., J. Qin, S. Wang, X. Li, H. Sun, and W. Chen (2020). Adsorption of Phenol on Commercial Activated Carbons: Modelling and Interpretation. *International Journal of Environmental Research and Public Health*, **17**(3); 789
- Zhang, F., S. Zhang, L. Chen, Z. Liu, and J. Qin (2021). Utilization of Bark Waste of Acacia Mangium: The Preparation of Activated Carbon and Adsorption of Phenolic Wastewater. *Industrial Crops and Products*, **160**; 113157
- Zhang, J., N. Liu, H. Gong, Q. Chen, and H. Liu (2022). Hydroxyl-functionalized Hypercrosslinked Polymers with Ultrafast Adsorption Rate as an Efficient Adsorbent for Phenol Removal. *Microporous and Mesoporous Materials*, **336**; 111836
- Zubair, M., I. Ihsanullah, H. A. Aziz, M. A. Ahmad, and M. A. Al-Harhi (2021). Sustainable Wastewater Treatment by Biochar/layered Double Hydroxide Composites: Progress, Challenges, and Outlook. *Bioresource technology*, **319**; 124128