

Facile Fabrication of Layered Double Hydroxide-Lignin for Efficient Adsorption of Malachite Green

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Abstract

Preparation of layered double hydroxide-lignin (lignin-Zn/Al) carried out by coprecipitation method. The FTIR spectra of lignin-Zn/Al displayed at 3448, 2939, 1620, 1381, 1118, 1041, and 601 cm^{-1} . The characteristic peaks are located at 10.1°, 19.1°, 20.1°, 29.4°, 33.9°, and 60.4°. The lignin-Zn/Al nitrogen adsorption-desorption isotherm showed a Type-IV curve, indicating that it had a mesoporous structure. The H3 kind of hysteresis loop also provides evidence for the presence of mesopores within the lignin-Zn/Al complex. Lignin-Zn/Al, lignin, and Zn/Al had pH_{pzc} values of 6.09, 3.01, and 6.09, respectively. Lignin-Zn/Al, lignin, and Zn/Al are positively charged when the pH of the solution is less than pH_{pzc}, and they are negatively charged when the pH of the solution is more than pH_{pzc}. The Langmuir and pseudo-second-order model best represented the MG adsorption onto all adsorbents. The lignin-Zn/Al, lignin, and Zn/Al were shown to have maximum Langmuir adsorption capacities of 83.034, 78.740, and 36.364 mg/g, respectively. Zn/Al adsorption capacity increased 2.28 times after being composited with lignin.

Keywords

Layered Double Hydroxide, Adsorption, Lignin, Malachite Green

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1. INTRODUCTION

The contamination brought on by the wastewater discharge of organic dyes has become a more prominent issue because of the industry's rapid development (Tang et al., 2022). In many industries, including papers, tannery, printing inks, clothing, and others, dyes are widely utilized. As a result, a lot of colorful wastewater is produced, and many organic dyes will have a major harmful impact on the environment and human health (Giri et al., 2022; Vigneshwaran et al., 2021). Malachite green (MG), a triphenylmethane cationic dye, is frequently used in the textile industry (Jin et al., 2022). However, even at low concentrations, MG has been discovered to have numerous toxicological side effects on human bodies, such as mutagenic, teratogenic, and cancerous consequences (Buvaneswari and Singanan, 2022; Sarkar et al., 2021).

Several cutting-edge methods, such as extraction (Raval et al., 2022), photodegradation (Puthukkara et al., 2022), membranes (Iqbal et al., 2022), oxidation combining ultrasonic and electrochemical (Ren et al., 2021), and adsorption (Moradi and Panahandeh, 2022), have been used to remove MG from aqueous medium over the past few decades. Adsorption has

garnered the most attention among these due to its straightforward functioning, design flexibility, practical recyclability, and excellent reliability. For the purpose of removing MG from an aqueous solution, numerous sophisticated adsorption materials have been developed recently, including *Costus woodsonii* (Van Tran et al., 2022), modified metal-organic frameworks (Dahlan et al., 2023), biowaste garlic peel (Pathania et al., 2022), and layered double hydroxide (Ahmad et al., 2023a). Layered double hydroxides (LDHs) are a type of 2D anionic clay that is composed of layers (Nazir et al., 2022). LDH has a structure similar to brucite with a large surface area, where M(II) is surrounded by six hydroxide ions, for instance, and forms an octahedral array that is connected to form an infinite 2D structure (Ahmed and Mohamed, 2022).

These adsorbents have excellent MG molecule adsorption performance, but for this purpose, sustainable, cost-effective adsorbents made from biomass are still required (Wang et al., 2018). Also, when compared to several previously described adsorbents, biomass-based adsorbents appear to be more environmentally friendly, cost-effective, and sustainable (Juleanti et al., 2021). Designing biomass-derived adsorbents to remove MG from aqueous media is therefore appealing. Lignin, an

amorphous high-molecular aromatic polymer, is the second most prevalent biomass component on the planet after cellulose (Zong et al., 2023). The pulp and paper industry currently produces about 50 million tons of lignin as a byproduct each year. The vast majority of lignin that has been burned up to this point has been done so to create energy, which has resulted in significant lignin resource waste (Du et al., 2023). The use of inexpensive, readily available industrial waste lignin to produce effective functional materials for environmental remediation is a great solution when taking into account greater lignin usage and water remediation (Wang et al., 2022). A three-dimensional network structure and the abundance of functional groups that include oxygen in lignin give it more potential for functionalization (Hamad et al., 2022).

In this work, the coprecipitation technique was used to prepare the lignin-Zn/Al. Many cutting-edge characterization techniques were used to examine the physicochemical characteristics of lignin-Zn/Al. Also, the potential of lignin-Zn/Al was examined, as well as its application to simulated textile wastewater.

2. EXPERIMENTAL SECTION

2.1 Materials

All chemicals were used without any further purification. Sodium chloride, sodium hydroxide, aluminum nitrate nonahydrate, chloride acid, and zinc nitrate hexahydrate were purchased from Sigma Aldrich and Merck. Lignin and distilled water were purchased from Tokyo Chemical Industry and Brataco, respectively.

2.2 Preparation Lignin-Zn/Al and Characterization

Lignin-Zn/Al was prepared by the coprecipitation method. Both 0.25 M aluminum nitrate nonahydrate and 0.75 M zinc nitrate hexahydrate were dissolved in 30 mL of distilled water, respectively. The solutions were added sodium hydroxide 2 M to pH 8 and stirred at 70°C for 4 h. Afterward, the Zn/Al added 3 g lignin was under continuous stirring for 3 days, filtered, and dried. The characterization of lignin-Zn/Al using Fourier Transfer Infra-Red (FTIR) (Shimadzu), X-Ray Diffractometer (XRD) (Rigaku), and Surface Area Analyzer (Quantachrome).

2.3 Adsorption Process of MG

Batch adsorption tests were conducted in a shaker. Investigations were into the effects of temperature (30–60°C), initial dye concentration (60–100 mg/L), contact time (10–180 min), and pH_{pzc} (2–11). Usually, 100 mL of beaker glass was filled with 30 mL of MG solution and 30 mg of lignin-Zn/Al. Liquid aliquots were obtained after adsorption and centrifuged. Then, the supernatant was examined using a UV-Vis spectrophotometer set to the maximum wavelength of 617 nm. Equation 1 was used to determine the concentration of MG.

$$q = \frac{(C_0 - C) \times V}{m} \quad (1)$$

Where q is adsorption capacity at t time (mg/g); C_0 and C are initial concentration and concentration for t time of MG, respectively (mg/L); V is the volume of MG (L); m is the mass of lignin-Zn/Al (g).

3. RESULTS AND DISCUSSION

FT-IR spectra of Zn/Al, lignin, and lignin-Zn/Al were presented in Figure 1. The FTIR spectra of lignin-Zn/Al displayed at 3448, 2939, 1620, 1381, 1118, 1041, and 601 cm^{-1} . The stretching vibration of -OH from Zn/Al is responsible for appearing of the broad bandwidth 3448 and 1620 cm^{-1} (Ahmad et al., 2023b). The band at 2939 cm^{-1} is stretching vibration of aliphatic -CH from lignin and the distinctive peak at bandwidth 1381 cm^{-1} is anion interlayer NO_3^- from Zn/Al (Zubair et al., 2022). The peak at 1118 and 1041 cm^{-1} are ascribable to C-O and C-O-C from lignin, respectively (Sun et al., 2022). The metal oxide bond vibration is attributed to the band at 601 cm^{-1} (Chen et al., 2022).

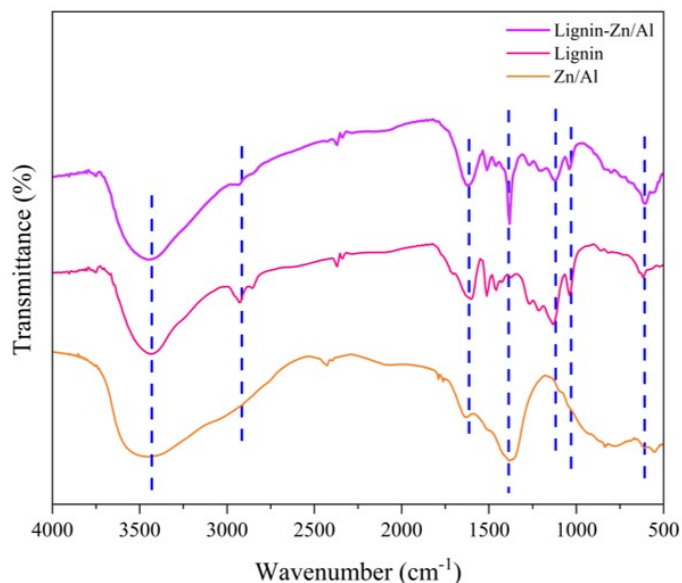


Figure 1. Fourier Transfer Infra-Red Results of Adsorbents

The usual Zn/Al XRD pattern can be seen in Figure 2, where the characteristic peaks are located at 10.1° and 20.1°, respectively, and correspond to the basal spacings of d003 and d006, respectively (Yuliasari et al., 2023). The 101 and 110 planes are responsible for two further linked peaks at 29.4° and 60.4°, respectively. The XRD of the lignin is depicted in Figure 2 and displays the distinctive peak of carbon material at 19.1° and 33.9° (Sturgeon et al., 2014). The XRD results of the lignin-Zn/Al mixture reveal the presence of distinctive Zn/Al and lignin reflections.

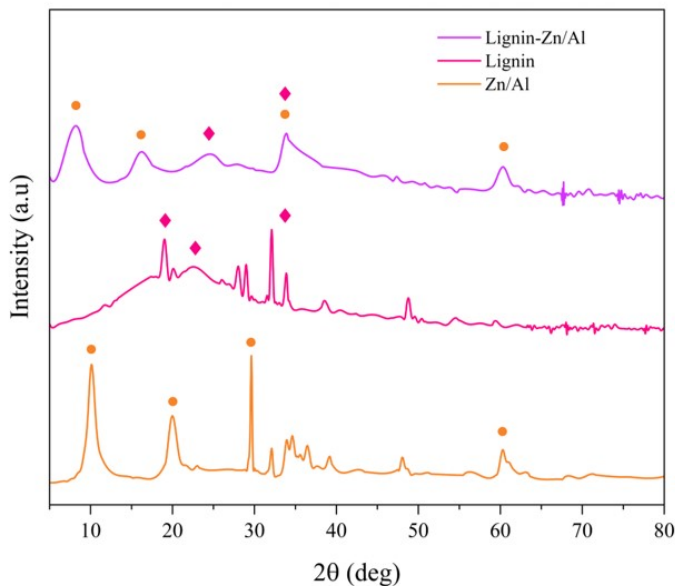
When evaluating the lignin-Zn/Al structure, the specific surface area and pore size are important factors. Table 3 quantitatively displays the lignin-Zn/Al, lignin, and Zn/Al pore's structure (d), surface area (S_{BET}), and pore volume (VP). The

Table 1. The Surface Area of Adsorbents

Adsorbent	S_{BET} (m ² /g)	d (nm)	VP (cm ³ /g)
Lignin-Zn/Al	7.125	1.960	0.007
Lignin	4.079	2.255	0.009
Zn/Al	1.968	27.687	0.006

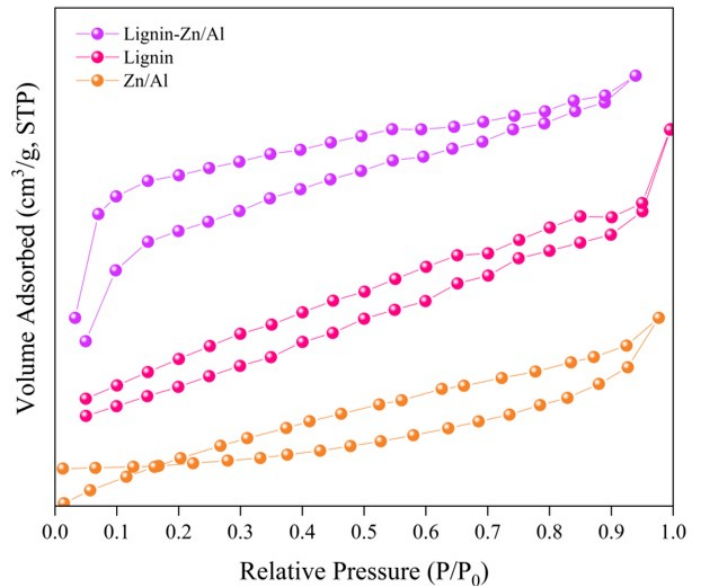
Table 2. Kinetic Data of Adsorbents

Adsorbent	Pseudo-First-Order				Pseudo-Second-Order		
	$Q_{e_{exp}}$ (mg/g)	$Q_{e_{calc}}$ (mg/g)	k_1 (min ⁻¹)	R^2	$Q_{e_{calc}}$ (mg/g)	k_2 (g/mg.min)	R^2
Lignin-Zn/Al	45.642	17.527	0.024	0.850	47.170	0.002	0.999
Lignin	39.892	29.336	0.036	0.941	44.053	0.002	0.993
Zn/Al	36.148	39.455	0.037	0.995	39.683	0.002	0.996

**Figure 2.** X-Ray Diffractometer Results of Adsorbents

results show that lignin-Zn/Al has an average surface area of 7.125 m²/g and pore sizes of 1.9620 ≈ 2 nm. The surface area of Zn/Al increase after combining with lignin. Our findings demonstrate the presence of mesopores in the lignin-Zn/Al structure, which have IUPAC-recommended diameter ranges of 2–50 nm (Heo et al., 2022). The N₂ adsorption/desorption curves and BJH (Barrett, Joyner, Halenda) pore size distributions of lignin-Zn/Al are shown in Figure 2. The lignin-Zn/Al nitrogen adsorption-desorption isotherm, as reported by IUPAC, showed a Type-IV curve, indicating that it had a mesoporous structure. The H3 kind of hysteresis loop also provides evidence for the presence of mesopores within the lignin-Zn/Al complex.

The pH_{pzc} of is the point when there is no charge at all.

**Figure 3.** Nitrogen Adsorption-Desorption Results of Adsorbents

When the pH of the solution is low, shaking causes H⁺ to migrate from the solution to the surface of the lignin-Zn/Al, lignin, and Zn/Al, raising the pH. When the solution has a high pH, H⁺ diffuses into the solution from the surface of lignin-Zn/Al, lignin, and Zn/Al. This reduces the pH of the solution. H⁺ ions do not migrate at the point where the initial and final pHs meet, indicating that pH_{pzc} is the point of convergence. Lignin-Zn/Al, lignin, and Zn/Al had pH_{pzc} values of 6.09, 3.01, and 6.09, respectively, as illustrated in Figure 4. Lignin-Zn/Al, lignin, and Zn/Al are positively charged when the pH of the solution is less than pH_{pzc}, and they are negatively charged when the pH of the solution is more than pH_{pzc}.

Table 2 lists the resulting parameters after the experimental

Table 3. Isotherm Data of MG Adsorption

Adsorbent	T (°C)	n	Freundlich		Q _{max}	Langmuir	
			kF	R ²		kL	R ²
Lignin-Zn/Al	30	5.230	1.431	0.828	78.125	0.233	0.994
	40	5.959	1.452	0.781	79.365	0.341	0.995
	50	7.930	1.490	0.645	83.333	0.723	0.996
	60	1.101	1.506	0.668	84.034	1.469	0.999
Lignin	30	1.978	1.228	0.878	67.568	0.076	0.955
	40	2.033	1.244	0.882	71.942	0.075	0.917
	50	2.439	1.291	0.928	72.464	0.093	0.985
	60	2.475	1.309	0.947	78.740	0.102	0.981
Zn/Al	30	0.876	2.037	0.880	23.310	0.121	0.982
	40	1.071	1.903	0.763	26.954	0.155	0.954
	50	1.388	1.789	0.732	30.675	0.203	0.956
	60	1.916	1.684	0.778	36.364	0.342	0.980

Table 4. Several Adsorbents to the Adsorption of MG

Adsorbent	Q _{max} (mg/g)	References
Lignin-Zn/Al	84.034	This study
Lignin	78.740	This study
Zn/Al	36.364	This study
<i>Avena sativa</i>	83	Banerjee et al. (2016)
Pine cone	111.1	Kavci (2021)
Graphene oxide aminated lignin aerogels	113.5	Chen et al. (2020)
Halloysite nanotube	74.95	Altun and Ecevit (2022)
Active carbons	58	Hijab et al. (2021)
Chitosan-zink oxide	11	Muinde et al. (2020)
PACT@ γ -Fe ₂ O ₃	62.89	Hasan et al. (2020)

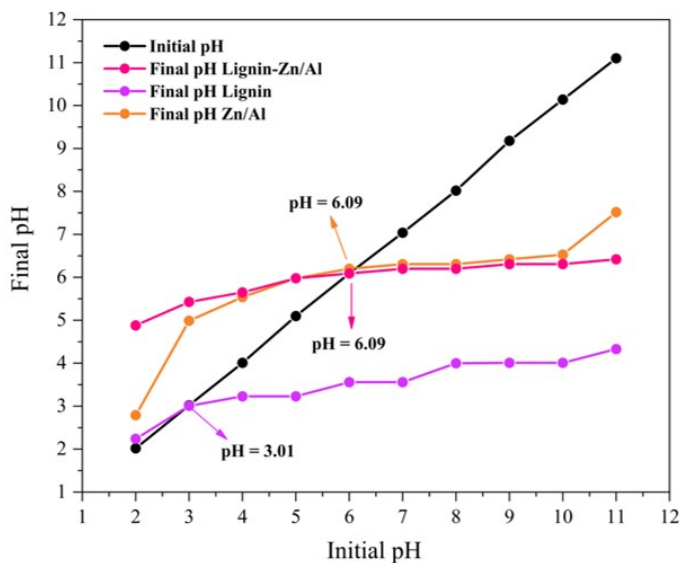


Figure 4. pHpzc of Lignin-Zn/Al, Lignin, and Zn/Al

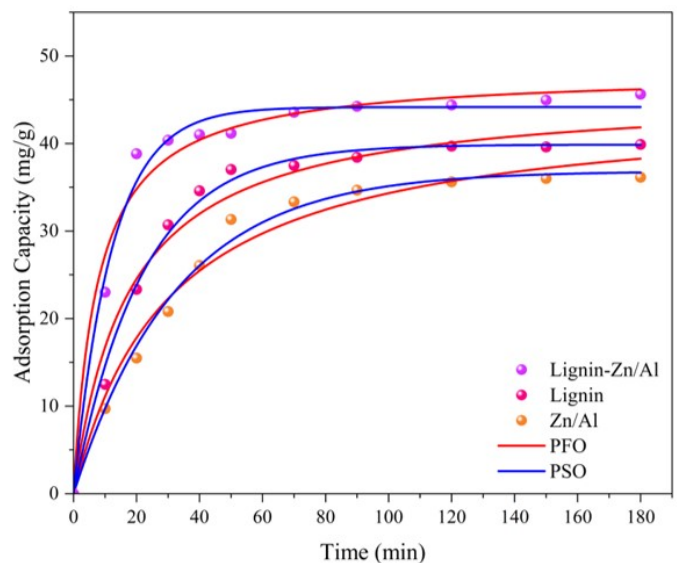


Figure 5. Contact Time Between Adsorbents and Adsorbate

data are fitted to the kinetics models. The pseudo-second-order equation is the most appropriate one to describe the adsorption kinetics of lignin-Zn/Al, lignin, Zn/Al for MG, as shown by the analysis of correlation coefficients shown in Table 2. All R^2 of the pseudo-second-order models are much closer to 1.0 than pseudo-first-order models. This suggests that the process of adsorption involves chemisorption (Rashed et al., 2022).

Isotherm studies were carried out to comprehend the MG adsorption equilibrium distribution between the aqueous and the lignin-Zn/Al, lignin, and Zn/Al phases. Due to their widespread acceptance and popularity for precisely characterizing adsorption processes, the Langmuir and Freundlich models were used to explain the adsorption process in order to achieve that. The parameters obtained after fitting the isotherm research data obtained at various temperatures into these models are shown in Table 3. The Langmuir model best represented the MG adsorption onto all adsorbents, according to the R^2 values for the three adsorbents. It follows that monolayer adsorption in nature Meng et al. (2019) would be a more accurate way to characterize the MG solution's adsorption onto lignin-Zn/Al, lignin, and Zn/Al. The lignin-Zn/Al, lignin, and Zn/Al were shown to have maximum Langmuir adsorption capacities of 83.034, 78.740, and 36.364 mg/g, respectively. Zn/Al adsorption capacity increased 2.28 times after being composited with lignin. Several adsorbents for the adsorption of MG are displayed in Table 4.

4. CONCLUSION

Preparation lignin-Zn/Al is successful by the coprecipitation method. The characterization by FTIR, XRD, and BET shows the physicochemical characteristics of lignin-Zn/Al. The adsorption process showed better results after Zn/Al and lignin were combined. This can be seen from the increase in the adsorption capacity of Zn/Al lignin by 2.28 times. Thus, lignin-Zn/Al can be one of the adsorbents for the malachite green adsorption process.

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